

LISTING OF CLAIMS

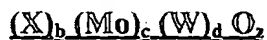
The following listing of claims will replace all prior versions and listings of claims in the application. Claims 1, 2, 3, 4 and 5 are currently submitted for amendment, along with claim 16, which is being made into two claims: amended claim 16 and added claim 20.

two reaction stages

1. (CURRENTLY AMENDED) A process for preparing a lubricating oil basestock containing at least about 90% saturates which comprises:

(a) passing a feedstock to a hydrotreating zone containing at least one hydrotreating reactor containing a hydrotreating catalyst;

(b) hydrotreating the feedstock in the presence of the hydrotreating catalyst under hydrotreating conditions wherein the hydrotreating catalyst comprises a bulk metal catalyst ~~comprising at least one non-noble Group VIII metal and two Group VIB metals and wherein said bulk metal catalyst comprises a non-noble Group VIII metal molybdate in which at least a portion but less than all of molybdenum is replaced by tungsten~~ represented by the formula:



wherein X is non-noble Group VIII metal, and the molar ratio of b: (c+d) is 0.5/1 to 3/1 to produce a hydrotreated feedstock; and

(c) fractionating the hydrotreated feedstock.

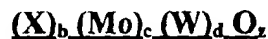
2. (CURRENTLY AMENDED) A process for preparing a lubricating oil basestock containing at least about 90% saturates which comprises:

(a) passing a feedstock to a first hydrotreating zone containing at least one hydrotreating reactor containing a first non-bulk metal hydrotreating catalyst;

(b) hydrotreating the feedstock in the presence of the first hydrotreating catalyst under first hydrotreating conditions wherein the first hydrotreating catalyst comprises at least one Group VIB and at least one non-noble Group VIII metal on a refractory oxide support to produce a first hydrotreated feedstock;

(c) passing at least a portion of the first hydrotreated feedstock to a second hydrotreating zone containing at least one hydrotreating reactor containing a second hydrotreating catalyst;

(d) hydrotreating the first hydrotreated feedstock in the second hydrotreating zone under second hydrotreating conditions wherein the second hydrotreating catalyst in said second hydrotreating zone comprises a bulk metal catalyst comprising ~~at least one non-noble Group VIII metal and two Group VIB metals and wherein said bulk metal catalyst comprises a non-noble Group VIII metal molybdate in which at least a portion but less than all of molybdenum is replaced by tungsten~~ represented by the formula:



wherein X is non-noble Group VIII metal, and the molar ratio of b: (c+d) is 0.5/1 to 3/1 to produce a hydrotreated feedstock; and

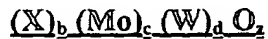
(e) fractionating the second hydrotreated feedstock.

3. **(CURRENTLY AMENDED)** A process for preparing a petroleum oil containing at least about 90% saturates which comprises:

(a) passing a feedstock to a hydrotreating zone containing at least one hydrotreating reactor containing a hydrotreating catalyst;

(b) hydrotreating the feedstock in the presence of the hydrotreating catalyst under hydrotreating conditions wherein the hydrotreating catalyst is a bulk metal catalyst ~~comprising at least one non-noble Group VIII metal and two Group~~

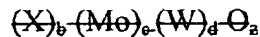
~~VIB metals and wherein said bulk metal catalyst comprises a non-noble Group VIII metal molybdate in which at least a portion but less than all of molybdenum is replaced by tungsten represented by the formula:~~



wherein X is non-noble Group VIII metal, and the molar ratio of b: (c+d) is 0.5/1 to 3/1 to produce a hydrotreated feedstock;

- (c) fractionating the hydrotreated feedstock to produce a first basestock;
- (d) passing the first basestock to a hydrogenation zone containing at least one hydrogenation reactor containing a hydrogenation catalyst;
- (e) hydrogenating the first basestock in the presence of the hydrogenation catalyst under hydrogenation conditions wherein the hydrogenation catalyst comprises at least one Group VIII metal; and
- (f) fractionating the hydrogenated product from step (e) to produce a petroleum oil containing at least about 90% saturates.

4. (CURRENTLY AMENDED) The process of claims 1, 2 or 3 wherein ~~the bulk metal catalyst is represented by the formula:~~



~~wherein X is non-noble Group VIII metal, the molar ratio of b: (c+d) is 0.5/1 to 3/1, the molar ratio of c:d is >0.01, and $z = [2b + 6(c+d)]/2$.~~

5. (CURRENTLY AMENDED) The ~~process of claim 4~~ processes of claims 1, 2 or 3 wherein the molar ratio of b:(c+d) is 0.75/1 to 1.5/1.

6. (ORIGINAL) The process of claim 5 wherein the molar ratio of b:(c+d) is 0.75/1 to 1.25/1.

7. (ORIGINAL) The process of claim 4 wherein the molar ratio of c:d is $>0.1/1$.

8. (ORIGINAL) The process of claim 7 wherein the molar ratio of c:d is $1/10$ to $10/1$.

9. (ORIGINAL) The process of claim 8 wherein the molar ratio of c:d is $1/3$ to $3/1$.

10. (ORIGINAL) The process of claim 3 wherein the hydrogenation catalyst further contains at least one Group VIB metal.

61 11. (ORIGINAL) The process of claim 3 wherein the Group VIII metal is a non-noble metal.

12. (ORIGINAL) The process of claim 11 wherein the non-noble metal is nickel.

13. (ORIGINAL) The process of claims 1 or 3 wherein the hydrotreating conditions comprise temperatures of from 250 to 400°C , hydrogen pressures of from 500 to 3500 psig (3549 to 24234 kPa), liquid hourly space velocities of from 0.1 to 5.0 and hydrogen treat gas rates of from 500 to 5000 scf/B (89 to 890 m^3/m^3).

14. (ORIGINAL) The process of claim 2 wherein the first hydrotreating conditions in the first hydrotreating zone comprise temperatures of from 250 to 400°C , hydrogen pressures of from 500 to 3500 psig (3549 to 24234 kPa), liquid

hourly space velocities of from 0.1 to 5.0 and hydrogen treat gas rates of from 500 to 5000 scf/B (89 to 890 m³/m³), and the second hydrotreating conditions in the second hydrotreating zone comprise temperatures of from 250 to 400 °C, hydrogen pressures of from 500 to 5000 psig (3549 to 24234 kPa), liquid hourly space velocities of from 0.1 to 5.0 and hydrogen treat gas rates of from 500 to 5000 scf/B (89 to 890 m³/m³).

15. (ORIGINAL) The process of claim 3 wherein the hydrogenation conditions comprise temperatures of from 150 to 400 °C, hydrogen pressures of from 500 to 3500psig (3549 to 24234 kPa), liquid hourly space velocities of from 0.1 to 5.0 and hydrogen treat gas rates of from 500 to 5000 scf/B (89 to 890 m³/m³).

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16. (CURRENTLY AMENDED) The process of claims ~~1, 2 or 3~~ wherein the petroleum oil is a white oil.

17. (ORIGINAL) The process of claim 16 wherein the white oil is a technical or medicinal white oil.

18. (ORIGINAL) The process of claim 4 wherein the non-noble metal is Ni or Co.

19. (ORIGINAL) The process of claim 4 wherein the non-noble metal is Ni.

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B. 20. (NEW) The process of claims 1 or 2 wherein the lubricating oil is
a white oil.
